## Claims

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- 1. A method for reducing the content of extractives of a high-yield pulp in a peroxide bleaching stage, said stage including peroxide bleaching and a subsequent dewatering or washing, said method comprising contacting the pulp in the peroxide bleaching with an organic stabilizer and in or after the peroxide bleaching with a surfactant, and thereafter subjecting the bleached pulp to said dewatering or washing for removing extractives along with the aqueous phase.
  - 2. The method according to claim 1 wherein the organic stabilizer and the surfactant are added to the pulp in the peroxide bleaching.
- 10 3. The method according to claim 1 wherein the organic stabilizer and the surfactant are added to the pulp before the peroxide bleaching.
  - 4. The method according to claim 1 wherein the surfactant is added to the pulp after the peroxide bleaching.
- 5. The method according to any of claims 1 to 4 wherein dilution water is added to the pulp between the peroxide bleaching and the dewatering or washing.
  - 6. The method according to claim 5 wherein the surfactant is added to the dilution water.
  - 7. The method according to any of claims 1 to 6 wherein the organic stabilizer comprises a polymeric stabilizer, such as a poly-alfa-hydroxyacrylic acid or a salt thereof or the corresponding polylactone, a homopolymer of acrylic acid, methacrylic acid or maleic acid or a copolymer of acrylic acid and/or methacrylic acid with an unsaturated dicarboxylic acid or a mixture of these polymers.
  - 8. The method according to any of claims 1 to 7 wherein the amount of the organic stabilizer is from 0.1 kg to 5 kg per ton dry pulp, preferably from 0.25 kg to 3 kg per ton dry pulp.
  - 9. The method according to any of claims 1 to 8 wherein the surfactant comprises an anionic surfactant, such as naphthalene sulphonate or lignosulphonate, or a non-ionic surfactant, such as an O/W emulsifier, f. ex. a fatty alcohol ethoxylate or alkyl phenol ethoxylate.

- 10. The method according to any of claims 1 to 9 wherein the amount of the surfactant is from 0.005 kg to 2 kg per ton dry pulp, preferably from 0.05 kg to 1 kg per ton dry pulp.
- 11. A method for producing bleached high-yield pulp having a reduced content of extractives comprising bleaching high-yield pulp with peroxide, the pulp being contacted with an organic stabilizer during the peroxide bleaching and with a surfactant during the peroxide bleaching or after the peroxide bleaching, and dewatering or washing the bleached pulp for removing extractives along with the aqueous phase and for producing bleached high-yield pulp having a reduced content of extractives.
  - 12. The method according to claim 11 wherein the organic stabilizer and the surfactant are added to the pulp in the peroxide bleaching.
  - 13. The method according to claim 11 wherein the organic stabilizer and the surfactant are added to the pulp before the peroxide bleaching.
- 15 14. The method according to claim 11 wherein the surfactant is added to the pulp after the peroxide bleaching.
  - 15. The method according to any of claims 11 to 14 wherein dilution water is added to the pulp between the peroxide bleaching and the dewatering or washing.
- 16. The method according to claim 15 wherein the surfactant is added to the dilution water.
  - 17. The method according to any of claims 11 to 16 wherein the organic stabilizer comprises a polymeric stabilizer, such as a poly-alfa-hydroxyacrylic acid or a salt thereof or the corresponding polylactone, a homopolymer of acrylic acid, methacrylic acid or maleic acid or a copolymer of acrylic acid and/or methacrylic acid with an unsaturated dicarboxylic acid or a mixture of these polymers.
  - 18. The method according to any of claims 11 to 17 wherein the amount of the organic stabilizer is from 0.1 kg to 5 kg per ton dry pulp, preferably from 0.25 kg to 3 kg per ton dry pulp.
- 19. The method according to any of claims 11 to 18 wherein the surfactant comprises an anionic surfactant, such as naphthalene sulphonate or lignosulphonate,

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or a non-ionic surfactant, such as an O/W emulsifier, f. ex. a fatty alcohol ethoxylate or alkyl phenol ethoxylate.

20. The method according to any of claims 11 to 19 wherein the amount of the surfactant is from 0.005 kg to 2 kg per ton dry pulp, preferably from 0.05 kg to 1 kg per ton dry pulp.

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